

Implementing a Subsea Oil-Water Separation System in Modelica

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Scope

- Create a Modelica model from scatch based in the Matlab model made by P. FürstTyvold for:
 - Subsea Gravity Separator
 - Cyclone Deoiler (Oil in water phase)
 - Cyclone Dewaterer (Water in oil phase)
- Create a connection system that allows the simulation of the system and connection with Modelica models.
- Simulating and optimizing the system.

Horizontal gravity separator.

• DRIVING FORCE: Gravity Based in Stokes law

$$v_{v} = \frac{2r_{d}^{2}(\rho_{d} - \rho)g}{9\mu(\alpha)}$$

OIL PHASE

Image: General conduction

Image: General conduction</

Тор

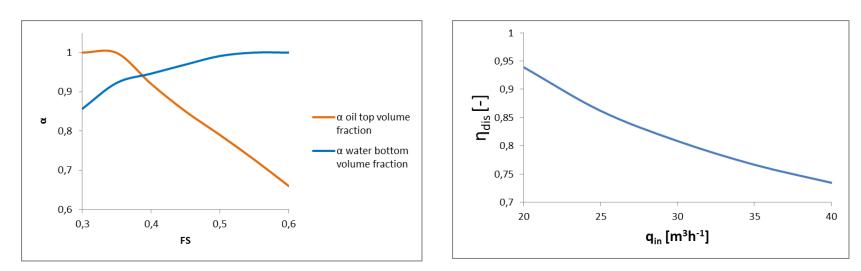
- Inlet flow rate
- Inlet oil volume fraction
- Flow split

Inputs:



Effect of the flow split and inlet flow rate in gravity separator

- Varying *FS*, $q_{in}=20m^3/h \alpha_{in}=0,4$ - Varying $q_{in},\alpha_{in}=0,40.4$ FS 0.4.



Dispersed efficiency

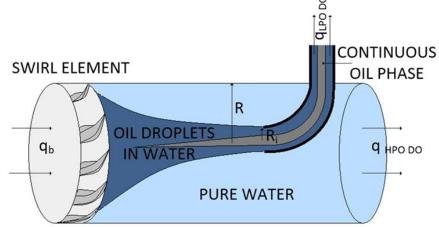
 $\eta_{dis} = \frac{\text{Oil flow rate in light output+Water flow rate in heavy output}}{\text{In lat flow rate in heavy output}}$

Inlet flow rate

DEOILER

• DRIVING FORCE: Tangential acceleration generated by static swirl element

Based in Stokes law Oil in water phase



Inputs:

- Inlet flow rate
- Inlet oil volume fraction
- Flow split
- Swirl element

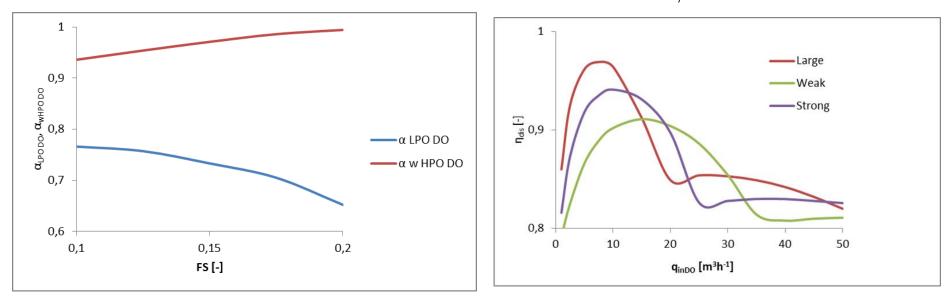
Outputs:

- Flow rate
- Oil volume fraction

Heavy phase Light phase

Effect of the flow split and inlet flow rate in deoiler/dewaterer

- Varying *FS*, q_{in} =13,65m³/h α_{in} =0,135 - Varying $q_{in}\alpha_{in}$ =FS= 0.135



Swirl element acts as a scaling factor of the tangential velocity

DEWATERER

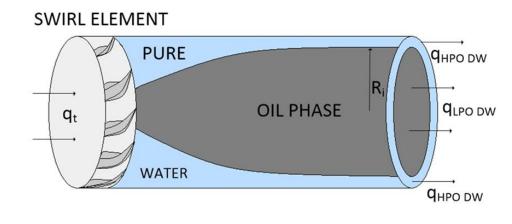
• DRIVING FORCE: Tangential acceleration generated by static swirl element.

Based in Stokes law

- Water in oil phase
- Now the droplets have higher density than continuous phase.

Inputs:

- Inlet flow rate
- Inlet oil volume fraction
- Flow split
- Swirl element



Outputs:

- Flow rate
- Oil volume fraction

Heavy phase Light phase

CONNECTING THE BLOCKS

 Connector – Setting up equations relating properties in connnected units

> Fluid connector variables: pressure, mass flow, mass fractions, enthalpy

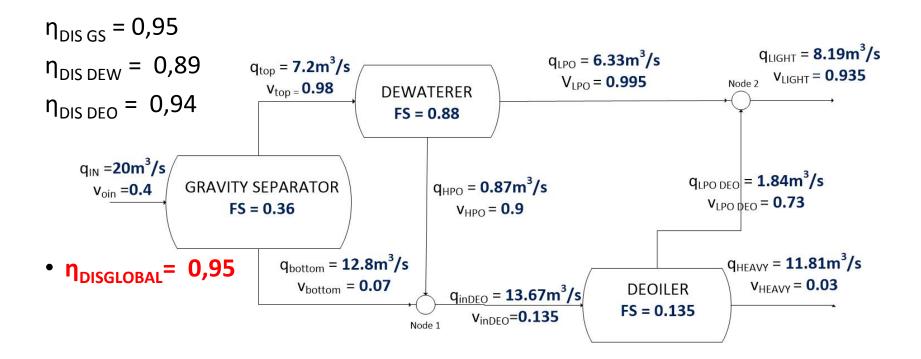
connector Flow_port
 import Oil_Water_Separation_System;
 import SI = Oil_Water_Separation_System.Units;
 SI.OilVolumeFraction volfracc "Volume fraction in the connection point";
 SI.VolumeFlowRate volflow "Volume flow rate in the connection point";
 end Flow_port;

And the blocks are connected together as follows:

9	equation
10	<pre>connect(GS.flowporttop,DEW.flowportindew);</pre>
11	<pre>connect(DEW.flowportoutdewH,NODE1.flowportinleta);</pre>

Separation system (I)

• Inlet conditions: $q_{in}=20m^3/h \alpha_{in}=0,4$ Objective $\alpha_{oil, water phase} = 0.03$ Maximize $\alpha_{oil oil phase}$ manipulating FS



SEPARATION SYSTEM (II)

• Inlet conditions: $q_{in}=20m^3/h \alpha_{in}=0,4$ Objective $\alpha_{oil, water phase} = 0.03$ Maximize $\alpha_{oil oil phase}$ manipulating FS Purity loss: 7,5% $q_{top} = 10.47 m^3/s$ $q_{LPO} = 9m^3/s$ $\eta_{DIS GS} = 0,87$ v_{top} = **0.78** V_{1PO} = 0.86 DEWATERER FS =0.85 $\eta_{DIS DEW} = 0.85$ $q_{gs} = = 21.57 \text{m}^3/\text{s}/$ Vogs =0.396 $q_{IN} = 20m^{3}/s$ **GRAVITY SEPARATOR v**_{oin} = **0.4** FS = 0.49Node 1 $q_{bottom} = 11m^3/s$ **v**_{bottom} = **0.03** $\eta_{\text{DISGLOBAL}} = 0,92$ $q_{HPO} = 1.57 \text{ m}^3/\text{s}$ V_{HPO} =0.39

Benefits of using Dymola

- Modeling and simulation platform .
- Graphical and text based coding .
- Flexibility :
 - -Transparent code
 - -Model structure
 - -Equation based
 - -Simple re-use of code .
- Object-oriented modeling language .
- Equation based, but allows using algorithms .