THERMODYNAMICS OF MIXTURES CONTAINING ALKOXYETHANOLS. XXVIII. LIQUID-LIQUID EQUILIBRIA FOR 2-PHENOXYETHANOL + SELECTED ALKANES

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ABSTRACT

The coexistence curves of the liquid-liquid equilibria (LLE) for systems of 2phenoxyethanol (2PhEE) with heptane, octane, cyclohexane, methylcyclohexane or ethylcyclohexane have been determined by the method of the critical opalescence using a laser scattering technique. All the curves show an upper critical solution temperature (UCST), have a rather horizontal top and their symmetry depends on the relative size of the mixture compounds. UCST values are higher for systems with linear alkanes than for solutions including cyclic alkanes. For these mixtures, the UCST increases with the size of the alkyl group attached to the cyclic part of the molecule. It is shown that interactions between alkoxyethanol molecules are stronger when the hydroxyether contains an aromatic group. Data are used to determine the critical exponent for the order parameter mole fraction. Values obtained are consistent with those provided by the Ising model or by the renormalization group theory.

KEYWORDS: LLE; 2-phenoxyethanol; alkanes/ UCST/ dipolar interactions

1. INTRODUCTION

Alkoxyethanols, CH₃-(CH₂)_n-O-(CH₂-CH₂O)_m-CH₂-CH₂OH, are a very interesting class of substances from a practical point of view, as oxygenated compounds are increasingly used as additives to gasoline due their octane-enhancing and pollution-reducing properties [1,2]. In addition, hydroxyethers are non-ionic amphiphile molecules, very effective as surfactants with a large number of applications [3,4]. On the other hand, alkoxyethanols are also of interest due to the presence of the O and OH groups in the same molecule, which allows self-association via inter- and intramolecular hydrogen bonds. Different spectroscopic techniques have been used to investigate the existence of intramolecular hydrogen bonds [5-8]. They are present at all conditions, even in vapour phase, whereas intermolecular H-bonds appear at higher concentrations of the cellosolve in liquid state. Thus, CH₃-(CH₂)_n-O-(CH₂)_p-OH molecules can form 5-, 6- and 7-membered rings for p = 2, 3 and 4, respectively. The formation of intramolecular H-bonds is more favourable when the molecules are in gauche conformations. The stability of these conformations decreases with increasing p, resulting in a smaller number of rotational conformations favourable for intramolecular H-bonds. On the other hand, the increasing ring size of the intramolecularly H-bonded monomers results in greater restriction to internal rotation and is responsible for increasing the entropy changes involved in the interconversion of the mentioned species into free monomers. Alkoxyethanols with two ether groups and m = 1 form 5-membered rings similar to those previously cited, but can also form 8-membered rings of quite different properties. This can be ascribed to the replacement of a methylene group by a less bulky oxygen atom which increases the stability of the ring system by decreasing the ring strain caused by crowding repulsions [6].

The formation of the intramolecular H-bonds leads to enhanced dipole-dipole interactions in solutions containing alkoxyethanols and alkanes in comparison to those present in mixtures with homomorphic alkanols [9]. The following evidences support this statement. a) The Trouton's constant of hydroxyethers, 99.58 J mol⁻¹ K⁻¹ [10], is closer to the value of non-self-associated compounds, 92.05 J mol⁻¹ K⁻¹ [10], than the value for 1-alkanols, 110.88 J mol⁻¹ K⁻¹ [10]. b) For a given alkane, the upper critical solution temperature (UCST) of the system including an alkoxyethanol is higher than that of the solution with the homomorphic 1-alkanol [9,11-14]. c) $H_{m,1}^{E,\infty}$ (2-alkoxyethanol(1) + alkane(2)) < $H_{m,1}^{E,\infty}$ (1-alkanol(1) + alkane(2)) [9,15], where $H_{m,1}^{E,\infty}$ is the excess partial enthalpy at infinite dilution of component i. For example, at 298.15 K, $H_1^{E,\infty}$ (2-methoxyethanol + heptane) = 17.6 kJ mol⁻¹ [15]. For 1-alkanol + alkane mixtures, this magnitude, independent of the alkane [16,17] is, at 303.15 K, 23.4 kJ mol⁻¹ for 1-hexanol [18], and 21.8 for 1-octanol [19]. This has been interpreted assuming that the hydroxyether molecules become free via the destruction of the intermolecular H-bonds on addition of the solvent molecules, and that each alkoxyethanol molecule forms an

intramolecular H-bond between the O and the OH group of the same molecule and thus stabilizes itself [15]. d) The molar excess enthalpies, H_m^E , of alkoxyethanol + alkane mixtures are higher than those of homomorphic 1-alkanol + alkane systems and the H_m^E curves for systems with alkoxyethanols are more symmetrical than those of alcoholic solutions, skewed towards low concentration of the self-associated compound [9].

In previous works, we have reported data on $H_{\rm m}^{\rm E}$, $C_{\rm p,m}^{\rm E}$ (molar excess heat capacities at constant pressure), $V_{\rm m}^{\rm E}$ (excess molar volumes), compressibilities and speeds of sound, vapour-liquid equilibria and LLE for binary mixtures of alkoxyethanols with different organic solvents (alkanes, 1-butanol, dibutylether, hydroxyethers) [11-14,20-23], and we have investigated these complex systems in terms of different theories: DISQUAC [9,24], ERAS [24,25], Flory [26-28], or the Kirkwood-Buff formalism [28]. As a continuation, we report here LLE data for 2-phenoxyethanol + alkane mixtures. This is useful to gain insight into the influence of the aromatic ring on the thermodynamic properties of alkoxyethanols.

2. EXPERIMENTAL

2.1 Materials

Heptane (142-82-5, puriss p.a. ≥ 0.995); octane (111-65-9, puriss p.a. ≥ 0.99); cyclohexane (110-82-7, puriss p.a. ≥ 0.995); methylcyclohexane (108-87-2, puriss p.a. ≥ 0.98) were from Fluka; ethylcyclohexane (167-891-7, puriss p.a. ≥ 0.99) and 2-phenoxyethanol (122-99) were from Aldrich (purities expressed in mass fraction). Prior to the measurements, the chemicals were stored over molecular sieves (UOP 3Å from Fluka). All these chemicals were used without other further treatment. The densities ρ at 298.15 K and atmospheric pressure were in good agreement with literature values (Table 1). Regarding to 2PhEE, no density data have been encountered for comparison. For a better characterization of this compound, we have determined its purity by GC analysis (≥ 0.995) and the density and refractive index, n_D , at different temperatures. At (293.15 and 303.15) K, $\rho/g \cdot cm^3 = 1.10692$ and 1.09916, while $n_D = 1.53907$, 1.53702 and 1.53501 at (293.15, 298.15 and 303.15) K, respectively. The water contents, determined by the Karl-Fischer method, were as follows (in mass fraction): $5 \cdot 10^{-6}$ for heptane, cyclohexane and methylcyclohexane, $26 \cdot 10^{-6}$ for octane, $46 \cdot 10^{-6}$ for ethylcyclohexane and $19 \cdot 10^{-6}$ for 2-phenoxyethanol.

2.2 Apparatus and Procedure

Mixtures were prepared by mass, with a weighing accuracy to \pm 0.00001 g, in Pyrex tubes of 1 cm i.d. and about 4 cm length, which then were immediately sealed by capping at

atmospheric pressure and room temperature. Conversion to molar quantities was based on the relative atomic mass table of 1996 issued by IUPAC in 1996 [29].

The coexistence curves of the binary mixtures were determined by the method of the critical opalescence. The samples in the sealed Pyrex tubes are placed in a thermostat bath a few hundredths of degree above the expected temperature. A red He-Ne laser (wavelength of 635 nm) is placed on one side of the equilibrium cell so that the light beam passing through the solution is focused on a photodiode (with its maximum response around 700 nm). When decreasing slowly the temperature (1.2 K h⁻¹), the growth of small drops of the dispersed liquid phase causes a diffusion of light during the transition. This results in a voltage variation in the photodiode output, measured by a digital multimeter model Agilent 34410A connected to a PC, which allows simultaneous accurate measurements of the transition temperatures. The temperature was measured with a precision of ± 0.001 K and estimated accuracy of ± 0.05 K by a Pt-1000 resistance connected to a multimeter model Philips PM2353, in such way that the resistance variations upon cooling are also registered in a PC. The thermometer was calibrated on the basis of the ITS-90 scale of temperature using the triple point of the water, and the fusion point of Ga. The separation temperatures were reproducible to ± 0.05 K for temperatures near the upper critical solution temperature. The precision of the equilibrium composition is expected to be better than 0.0005 in mole fraction. The weighing technique gives a precision better than 0.0001 in mole fraction. but this is reduced slightly due to partial evaporation of the more volatile component to the free volume of the ampoule ($\approx 1.4 \text{ cm}^3$).

3. **RESULTS**

Table 2 lists the direct experimental results of the liquid-liquid equilibrium temperatures T vs. the mole fraction of 2PhEE, x_1 , for the investigated mixtures (Figs. 1,2).

All the systems show an UCST. The LLE coexistence curves have a flat maximum, and their symmetry depends on the relative size of the mixture compounds (Figs. 1,2). Thus, an increase of the molar volume of the alkane leads to LLE curves which become progressively skewed towards increasing x_1 values (Figs. 1,2). As consequence, the representation of the equilibrium temperatures vs. x_1 or vs. Φ_1 , the volume fraction ($\Phi_1 = x_1V_i/(x_1V_1 + x_2V_2)$, V_i , molar volume of component i) differ for the octane system (Fig. 1).

The coordinates of the critical points, x_{1c} and T_c (Table 3), were obtained by reducing the experimental data with the equation [30,31]

$$T/K = T_c/K + k |y - y_c|^m$$
⁽¹⁾

where

$$y = \frac{\alpha x_1}{1 + x_1(\alpha - 1)} \tag{2}$$

$$y_c = \frac{\alpha x_{lc}}{1 + x_{lc} \left(\alpha - 1\right)} \tag{3}$$

In eqs 1 to 3, *m*, *k*, α , *T*_c and *x*_{1c} are the coefficients to be fitted to the experimental results. When $\alpha = 1$, eq (1) is similar to the well-known equation [32-35]:

$$\Delta \lambda = B \tau^{\beta} \tag{4}$$

where $\Delta \lambda_1 = \lambda_1' - \lambda_2''$ is the so-called order parameter, which can be any density variable in the conjugate phase [35] (mole fraction, volume fraction; in our case $\lambda_1 = x_1$), τ is the reduced temperature $(T_c - T)/T_c$ and β a critical exponent corresponding to this order parameter. The β value depends on the theory applied to its determination [33-37]. More details are given below.

The fitting was performed using the Marquardt algorithm [38] with all the points weighted equally. Results are collected in Table 3. Also listed is the standard deviation defined by:

$$\left(\sigma\left(T\right)/K\right) = \left[\sum \left(T_{\exp,i} - T_{\operatorname{calc},i}\right)^{2}/(N-n)\right]^{1/2}$$
(5)

where N and n stand for the number of data points and the number of fitted parameters, respectively. We note that eq 1 fits well the experimental data.

4. **DISCUSSION**

We note that the UCSTs of mixtures involving linear alkanes are higher than those of systems with cyclic alkanes (Table 3). The same trend is observed in solutions containing other alkoxyethanols. Thus, for 2-methoxyethanol (2ME) mixtures, UCST(cyclohexane) = 294.58 K [11] < UCST(hexane) = 311.19 K [11] and UCST(methylcyclohexane) = 297.34 K [13] < UCST(heptane) = 319.74 K [13]. This reveals that cyclic alkanes break more easily interactions between alkoxyethanol molecules than *n*-alkanes. Consequently, UCST of 2PhEE solutions increases in the sequence: cyclohexane < methylcyclohexane < ethylcyclohexane (Table 3, Fig 2), as the size of the alkyl group attached to the cyclic part of the molecule increases in the same order. For a similar reason, UCST(heptane) < UCST(octane) (Table 3). The increase of UCST

with the chain length of the *n*-alkane is also encountered in mixtures with 2ME, 2-ethoxyethanol (2EE), or 2-(2-ethoxyethoxy)ethanol (22EEE) [11,12,14].

It is interesting to compare UCST of binary systems containing different alkoxyethanols and the same alkane. Thus, for systems with heptane, UCST increases in the order: 261.15 K (2EE) [39] < 287.97 K (22EEE) [14] < 319.74 K (2ME) [13]] < 367.57 K (2PhEE) (this work). This indicates that interactions between like molecules are enhanced by the presence of the aromatic group in 2-phenoxyethanol.

As previously mentioned, the β value in eq. (4) depends on the theory applied for its determination. The renormalization group approach yields 0.325, while the Ising model gives 0.312. The classical model gives 0.5 [32-37]. Application of eq. (1) is rather difficult because it is needed to know the composition in conjugate phases to determine the order parameter. The experimental method followed in this work suffers from the drawn-back that the equilibrium temperatures of the two coexisting compositions are not determined simultaneously. Here, we have used a modification of eq. (1) to estimate β , which is obtained taking $\alpha = 1$ [32,40,41]:

$$T / K = T_c / K + k' |x_1 - x_{1c}|^{1/\beta}$$
(6)

When applying this equation, firstly, it is necessary to determine its validity range. This was done by analyzing the data for various choices of range [42]. Thus, eq. (6) was used for temperature ranges $(T_c - T)/K= 1.96, 1.63, 1.57, 1.94$ and 1.80 for the systems with heptane, octane, cyclohexane, methylcyclohexane, or ethylcyclohexane, respectively. The fitting of the four parameters in eq. (6), T_c , x_{lc} , k', and $1/\beta$ was developed as previously. The standard deviations were (0.05, 0.05, 0.05, 0.02 and 0.02) K for the mixtures in the same order as cited above. The β values calculated were: 0.307 (heptane); 0.299 (octane); 0.362 (cyclohexane), 0.314 (methylcyclohexane) and 0.304 (ethylcyclohexane). Similar results have been obtained for systems such as: methanol + heptane, or + carbon disulphide, acetic anhydride + heptane, + cyclohexane, or + carbon disulphide [40,41]. It is interesting to note that no improvement is reached when replacing the mole fraction by the volume fraction, which is probably due to the similar molar volumes of the mixtures components.

5. CONCLUSIONS

LLE coexistence curves were determined for mixtures of 2PhEE with heptane, octane, cyclohexane, methylcyclohexane or ethylcyclohexane. UCST values are higher for systems with linear alkanes than for solutions including cyclic alkanes. For the latter mixtures, the UCST

increases with the size of the alkyl group attached. Interactions between alkoxyethanol molecules are stronger when the hydroxyether contains an aromatic group.

6. **REFERENCES**

- C. Zeberg-Mikkelsen, L. Lugo, J. García, J. Fernández, Volumetric properties under pressure for the binary system ethanol + toluene Fluid Phase Equilib., 235 (2005) 139-151.
- [2] R. Csikos, I. Pallay, J. Laky, E.D. Radchenko, B.A. Englin, J.A. Robert, Low-lead fuel with MTBE and C4 alcohols Hydrocarbon Process., 55 (1976) 121-125.
- [3] A.V. Deo, N.R. Sanjana, S.B. Kulkarri, M.K. Ghrapurey, A.B. Biswas, Nature (London), 187 (1960) 870-871.
- [4] M.I. Davis, Thermodynamic and related studies of amphiphile + water systems, Chem. Soc. Rev., 22 (1993) 127-134.
- [5] L.P. Kuhn, R.A. Wires, The Hydrogen bond. VI. Equilibrium between hydrogen bonded and nonbonded conformation of α,ω-diol monomethyl ethers, J. Am. Chem. Soc., 86 (1964) 2161-2165.
- [6] L.S. Prabhuminarishi, Self association behaviour of α, ω -diol monoalkyl ethers J. Chem. Soc. Faraday Trans. 2, 74 (1978) 1567-1572.
- [7] W. Caminati, E.B. Wilson, Internal hydrogen bond, torsional motion, and molecular properties of 2-methoxyethylamine by microwave spectroscopy : methyl barrier to internal rotation for 2-methoxyethanol, J. Mol. Spectrosc., 81 (1980) 356-372.
- [8] R.L. Brinkley, R. Gupta, Intra- and intermolecular hydrogen bonding of 2methoxyethanol and 2-butoxyethanol in *n*-hexane, Ind. Eng. Chem. Res., 37 (1998) 4823-4827.
- [9] J.A. González, J.C. Cobos, F.J. Carmona, I. García de la Fuente, V.R. Bhethanabotla, S.W. Campbell, Thermodynamics of mixtures containing alkoxyethanols. Part XV. DISQUAC characterization of systems of alkoxyethanols with *n*-alkanes or cyclohexane, Phys. Chem. Chem. Phys., 3 (2001) 2856-2865.
- [10] S.V. Vinogradov, R.H. Linnell, Hydrogen Bonding, Van Nostrand, Reinhold, New York, 1971.
- [11] M.A. Rubio, J.A. González, I. García de la Fuente, J.C Cobos, Thermodynamic properties of *n*-alkoxyethanols+organic solvents mixtures: VIII. Liquid–liquid equilibria of systems containing 2-methoxyethanol and alkanes (C_6H_{12} and $CH_3-(CH_2)_u-CH_3$, u = 3,4,6,8), Fluid Phase Equilib., 143 (1998) 111-123.
- [12] M.A. Rubio, J.A. González, I. García de la Fuente, J.C. Cobos, Thermodynamic properties of *n*-alkoxyethanols + organic solvent mixtures. IX. Liquid–liquid equilibria

of systems containing 2-methoxyethanol or 2-ethoxyethanol and selected *n*-alkanes, J. Chem. Eng. Data, 43 (1998) 811-814.

- [13] F.J. Carmona, J.A. González, I. García de la Fuente, J.C. Cobos, Thermodynamic properties of *n*-alkoxyethanols + organic solvent xixtures. X. Liquid–liquid equilibria of systems containing 2-methoxyethanol, 2-(2methoxyethoxy)ethanol or 2-(2-ethoxyethoxy)ethanol, and selected alkanes, J. Chem. Eng. Data, 44 (1999) 892-895.
- [14] R. Martínez, J.A. González, I. García de la Fuente, J.C. Cobos, Thermodynamic properties of *n*-alkoxyethanols + organic solvent mixtures. XIV. Liquid–liquid equilibria of systems containing 2-(2-ethoxyethoxy)ethanol and selected alkanes, J. Chem. Eng. Data, 45 (2000) 1036-1039.
- [15] F. Kimura, S. Murakami, R. Fujishiro, Y. Toshiyasu, Molar excess enthalpies of alpha, omega-alkanediol monoalkyl ether + heptane systems at 298 K, Bull. Chem. Soc. Jpn., 50 (1977) 791-794.
- [16] R.H. Stokes, C. Burfitt, Enthalpies of dilution and transfer of ethanol in non-polar solvents, J. Chem. Thermodyn., 5 (1973) 623-631.
- [17] J. A. González, I. García de la Fuente, J. C. Cobos, C. Casanova, A characterization of the aliphatic/hydroxyl interactions using a group contribution model (DISQUAC), Ber. Bunsenges. Phys. Chem., 95 (1991) 1658-1668.
- [18] M.K. Woycicka, W.M. Recko, Heats of mixing of propanol and hexanol with hydrocarbons at high dilution, Bull. Acad. Pol. Sci., Ser. Sci. Chim., 20 (1972) 783-788.
- [19] C.G. Savini, D.R. Winterhalter, H.C. Van Ness, Heats of mixing of some alcoholhydrocarbon systems, J. Chem. Eng. Data, 10 (1965) 168-171.
- [20] J.C. Cobos, C. Casanova, Excess enthalpies of some cellosolves with 1-butanol at 298.15K, Fluid Phase Equilib., 20 (1985) 155-160.
- [21] J.C. Cobos, C. Casanova, G. Roux-Desgranges, J.-P.E. Grolier, Excess properties of mixtures of some *n*-alkoxyethanols with organic solvents II. V_m^E and C_{p,m}^E with di-*n*butylether at 298.15 K, J. Chem. Thermodyn., 19 (1987) 791-796
- [22] J. Carmona, V.R. Bhethanabotla, S.W. Campbell, J.A. González, I. García de la Fuente,
 J.C. Cobos, Thermodynamic properties of (*n*-alkoxyethanols + organic solvents). XII.
 Total vapour pressure measurements for (*n*-hexane,*n*-heptane or cyclohexane + 2 methoxyethanol) at different temperatures, J. Chem. Thermodyn., 33 (2001) 47-59.
- [23] I. Mozo, I. García de la Fuente, J.A. González, J.C. Cobos, Thermodynamics of mixtures containing alkoxyethanols. Part XX. Densities, excess molar volumes, speeds of sound

and isothermal compressibilities for 2-alkoxyethanol + dibutylether systems at 293.15, 298.15 and 303.15 K, J. Mol. Liq., 129 (2006) 155-163.

- [24] J.A. González, J.C. Cobos, I. Mozo, I. García de la Fuente, Thermodynamics of mixtures containing alkoxyethanols: Part XIX. Systems with linear monoethers or 1-alkanols, J. Mol. Liq., 126 (2006) 99-110.
- [25] J.A. González, S. Villa, N. Riesco, I. García de la Fuente, J.C. Cobos, Thermodynamics of mixtures containing alkoxyethanols. Part XVII. ERAS characterization of alkoxyethanol + alkane systems. Can. J. Chem., 81 (2003) 319-329.
- [26] N. Riesco, S. Villa, J.A. González, I. García de la Fuente, J.C. Cobos, Thermodynamic properties of *n*-alkoxyethanols+organic solvent mixtures: XIII. Application of the Flory theory to 2-methoxyethanol + *n*-alkoxyethanols systems, Thermochim. Acta, 362 (2000) 89-97.
- [27] J.A. González, I. Mozo, I. García de la Fuente, J.C. Cobos, N. Riesco, Thermodynamics of mixtures containing alkoxyethanols: Part XXVII. Predictions on isobaric thermal expansion coefficients, compressibilities and speeds of sound from the Flory theory, Thermochim. Acta, 476 (2008) 20-27.
- [28] J.A. González, N. Riesco, I. Mozo, I. García de la Fuente, J.C. Cobos, Thermodynamics of mixtures containing alkoxyethanols. XXI. Application of the Flory theory to the study of orientational effects in systems with dibutyl ether or 1-butanol, Ind. Eng. Chem. Res., 46 (2007) 1350-1359
- [29] IUPAC: Atomic weights of the elements 1995 (IUPAC technical report), Pure Appl. Chem., 68 (1996) 2339-2359.
- [30] J.B. Ott, I.F. Holscher, G.M. Schneider, (Liquid + liquid) phase equilibria in (methanol + heptane) and (methanol + octane) at pressures from 0.1 to 150 MPa, J. Chem. Thermodyn., 18 (1986) 815-826.
- [31] U. Haarhaus, G.M. Schneider, (Liquid + liquid) phase equilibria in (methanol + butane) and (methanol + pentane) at pressures from 0.1 to 140 MPa, J. Chem. Thermodyn., 20 (1988) 1121-1129.
- [32] J.S. Rowlinson, F.L. Swinton. Liquids and Liquid Mixtures, 3rd ed., Butterworths, London, 1982.
- [33] J.P. Novak, J. Matous, J. Pick. Liquid-Liquid Equilibria, Elsevier: Amsterdam, 1987.
- [34] H.E. Stanley. Introduction to Phase Transitions and Critical Phenomena, Clarendon Press, Oxford, 1971.
- [35] S.C. Greer, M.R. Moldover, Thermodynamic anomalies at critical-points of fluids, Ann. Rev. Phys. Chem., 32 (1981) 233-265.

- [36] N. Nagarjan, A. Kumar, E.S.R. Gopal, S.C. Creer, Liquid-liquid critical phenomena. The coexistence curve of *n*-heptane-acetic anhydride, J. Phys. Chem., 84 (1980) 2883-2887.
- [37] S.C. Greer, Coexistence curves at liquid-liquid critical-points ising exponents and extended scaling Phys. Rev. A, 14 (1976) 1770-1780.
- [38] P.R. Bevington, Data Reductions and Error Analysis for the Physical Sciences. McGraw-Hill Book Co., London, 1969.
- [39] A.W. Francis, Critical solution temperatures, Advances in Chemistry Series 31, American Chemical Society: Washintgton D.C., 1961.
- [40] B. Viswanathan, K. Govindarajan, E.S.R. Gopal, Critical behavior of specific-heat and coexistence curve in binary liquid system methanol + heptane, Ind. J. Pure. Appl. Chem., 11 (1972) 157-162.
- [41] A. Sivaraman, A.K. Bandyopadyay, V.C. Padaki, Pressure dependence of the critical coexistence curve in three binary liquid mixtures, Proc. Nucl. Phys. Solid. State, Phys. Symp., 20C (1977) 327-329.
- [42] S.C. Greer, Liquid-liquid critical phenomena, Acc. Chem. Res. 11 (1978) 427-432.
- [43] J.A. Riddick, W.B. Bunger, T.K. Sakano. Organic Solvents, Techniques of Chemistry. Weissberger, A. Ed., Wiley: NewYork, Vol. II, 1986.

7. LIST OF SYMBOLS

k,m	parameters in eq.	(1)
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x mole fraction in liquid phase

Greek letters

α	parameter in eq.(1)
β	critical exponent for the order parameter (mole fraction)
ρ	density
σ	relative standard deviation (eq. 5)
τ	reduced temperature
Subscripts	
c	critical point

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TABLE 1

Compound	ho / (g·cm ⁻³)		
-	Experimental	Literature [43]	
2-Phenoxyethanol	1.10341		
Heptane	0.67971	0.67946	
Octane	0.69876	0.69862	
Cyclohexane	0.77395	0.77389	
Methylcyclohexane	0.76478	0.76506	
Ethylcyclohexane	0.78402	0.7839	

Comparison of experimental densities ρ with literature for pure liquids at T = 298.15 K

TABLE 2

Experimental liquid-liquid equilibrium temperatures for 2-phenoxyethanol(1) + alkane(2) mixtures.

<i>x</i> ₁	T/K	<i>x</i> ₁	T/K			
2-phenoxyethanol(1) + heptane(2)						
0.2089	361.59	0.4602	367.56			
0.2389	363.41	363.41 0.4752 3				
0.2618	364.76	0.4976	367.60			
0.2810	365.64	0.5112	367.45			
0.3007	366.37	0.5250	367.35			
0.3379	367.02	0.5466	367.28			
0.3741	367.38	0.5926	366.41			
0.3954	367.52	0.6273	365.13			
0.4232	367.54	0.6537	363.48			
0.4297	367.53	0.6858	361.45			
0.4511	367.59					
	2-phenoxyeth	anol(1) + octane(2)				
0.2774	365.92	0.4740	369.25			
0.2914	366.52	0.4998	369.25			
0.2992	366.86	0.5221	369.16			
0.3196	367.62	0.5446	369.17			
0.3382	368.19	0.5700	368.98			
0.3561	368.46	0.5914	368.80			
0.3719	368.84	0.6195	368.26			
0.3958	368.95	0.6406	367.64			
0.4208	369.12	0.6687	366.74			
0.4448	369.18	0.6894	365.69			
	2-phenoxyethano	l(1) + cyclohexane(2)				
0.1166	310.55	0.3837	314.83			
0.1264	311.48	0.4145	314.70			
0.1562	312.96	0.4336	314.40			
0.1851	313.90	0.4465	314.33			
0.2063	314.36	0.4642	314.04			
0.2264	314.63	0.4788	313.81			
0.2555	314.88	0.4959	313.36			
0.2855	314.93	0.5134	312.83			

TABLE 2	(continued)
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0.3246	314.93	0.5370	312.03
0.3546	314.92	0.5899	309.22
0.3701	314.86		
	2-phenoxyethanol(1) +	- methylcyclohexane(2	2)
0.1527	320.99	0.4077	325.53
0.1821	322.82	0.4339	325.49
0.2155	324.17	0.4586	325.39
0.2404	324.77	0.4807	325.20
0.2744	325.22	0.5013	324.91
0.2994	325.47	0.5278	324.44
0.3176	325.51	0.5539	323.65
0.3460	325.54	0.5845	322.38
0.3771	325.59	0.6144	321.13
	2-phenoxyethanol(1)	+ ethylcyclohexane(2)	1
0.1990	327.34	0.4255	330.37
0.2106	327.79	0.4491	330.31
0.2246	328.36	0.4756	330.32
0.2499	329.09	0.4994	330.19
0.2748	329.63	0.5238	330.05
0.2971	329.97	0.5497	329.70
0.3252	330.20	0.5710	329.36
0.3493	330.28	0.6005	328.57
0.3746	330.35	0.6233	327.79
0.4027	330.36	0.6350	327.19

TABLE 3

N^{a}	т	K	α	$T_{\rm c}/{ m K}$	x_{1c}	σ/K	
	2-phenoxyethanol(1) + heptane(2)						
21	3.16	-579.	0.954	367.6	0.449	0.09	
2-phenoxyethanol(1) + octane(2)							
20	3.17	-509	1.005	369.2	0.481	0.05	
	2-phenoxyethanol(1) + cyclohexane(2)						
21	3.34	-447	1.513	314.9	0.319	0.06	
2-phenoxyethanol(1) + methylcyclohexane(2)							
18	3.22	-436	1.310	325.6	0.369	0.06	
2-phenoxyethanol(1) + ethylcyclohexane(2)							
20	3.30	-462	1.006	330.3	0.415	0.03	

Coefficients in eq. (1) for the fitting of the (x_1, T) pairs given in Table 2 for 2-phenoxyethanol(1) + alkane(2) mixtures; σ is the standard deviation defined by eq 5.

^anumber of experimental data points.

CAPTION TO FIGURES

- **FIG. 1** LLE for the 2-phenoxyethanol(1) + octane(2) mixture. Points, experimental results (this work): T vs. x_1 (•) or vs. Φ_1 (O). Solid lines, results from the fitting equation (1) using the (x_1 , T) pairs.
- **FIG. 2** LLE for the 2-phenoxyethanol(1) + alkane(2) mixtures. Point, experimental results (this work). Full symbols, $T \text{ vs. } x_1$: (•), cyclohexane, (•), methylcyclohexane; (•), ethylcyclohexane; (O), $T \text{ vs. } \Phi_1$ for the cyclohexane system. Solid lines, results from the fitting equation (1) using the (x_1 , T) pairs.



FIG. 1



