

Thermodynamics of 2-alkanol + polar organic solvent mixtures. I. Systems with ketones, ethers or organic carbonates

Juan Antonio González*, Fernando Hevia, Luis Felipe Sanz, Daniel Lozano-Martín, Isaías García de la Fuente

G.E.T.E.F., Departamento de Física Aplicada, Facultad de Ciencias, Universidad de Valladolid, Paseo de Belén, 7, 47011 Valladolid, Spain



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ABSTRACT

The mixtures 2-propanol or 2-butanol + *n*-alkanone, or + acetophenone, or + linear monoether, or + cyclic ether, or + linear organic carbonate, or + propylene carbonate have been investigated using thermodynamic data, and in terms of the Flory theory, and the Kirkwood-Buff integrals. The data considered are: excess molar enthalpies (H_m^E), volumes, entropies, and the temperature dependence of H_m^E . The enthalpy of the 2-alkanol-solvent interactions have been determined, and the different contributions to H_m^E discussed. It is shown that H_m^E values of the 2-alkanol (fixed) + *n*-alkanone, or + linear carbonate mixtures change in the same manner that for *n*-alkanone, or linear carbonate + *n*-alkane (fixed) systems. In contrast, H_m^E values of 2-alkanol (fixed) + linear monoether or + *n*-alkane mixtures change similarly. This set of results suggests that solvent–solvent interactions are determinant in systems with *n*-alkanone or linear carbonate, while interactions between alcohol molecules are determinant in mixtures with linear monoethers. According to the Flory model, orientational effects in systems with a given 2-alkanol become weaker in the sequence: linear monoether > linear organic carbonate > *n*-alkanone, and are stronger in solutions with a cyclic monoether than in those with cyclic diethers, and in systems with acetophenone or propylene carbonate than in the mixtures with the corresponding linear solvents. Results obtained from the Kirkwood-Buff integrals are consistent with these findings. The application of Flory model reveals that orientational effects are similar in systems with 1- or 2-alkanols, with the exception of solutions with linear monoethers, where such effects are stronger in mixtures containing 1-alkanols. For the examined systems, the formalism of the Kirkwood-Buff integrals makes no meaningful distinction between solutions with 1-alkanols or 2-alkanols.

1. Introduction

Hydrogen bonding is fundamental in basic sciences and in industrial applications. In addition, this attractive interaction together with the C–C interactions are essential for humans since water, a H-bonding compound, is crucial for the maintenance and development of life. It is well-known that alcohols are self-associated molecules which form molecular aggregates when are mixed with inert and non-polar solvents. The size and shape (linear, cyclic) of the formed clusters can be investigated using, e.g., thermodynamic data [1–5], or a variety of different spectroscopic techniques [6–10] or dielectric measurements [11–16]. On the other hand, experimental data have been employed to investigate this type of solutions by means of different models: association theories, [4,17,18], group contribution models [19,20], equations of state [21],

the Kirkwood correlation factor [12,18], or the Kirkwood-Buff integrals [22,23], amongst others.

We have studied changes produced in the alcohol network and orientational effects in systems with 1-alkanol and ether [24,25], or *n*-alkanone [26], or linear organic carbonate [27], or + nitrile [28] on the basis of the thermodynamic data available, and using different models such as: Flory [29], the Kirkwood-Buff integrals, or the formalism of the concentration-concentration structure factor [30]. The main conclusion of these studies is that random mixing is a good approximation for describing the behavior of many of the mentioned solutions. As a continuation of these works, we pay now attention to 2-alkanol + polar organic solvent mixtures. In the present research the solvents considered are: *n*-alkanones (propanone, 2-butanone, 2-pentanone, 3-pentanone), acetophenone, linear monoethers (dipropyl ether (DPE) and dibutyl

* Corresponding author.

E-mail address: jagl@termo.uva.es (J. Antonio González).

ether (DBE)), cyclic ethers (oxolane (THF), oxane (THP), 1,4-dioxane, 1,3-dioxolane) and organic carbonates (dimethyl carbonate (DMC), diethyl carbonate (DEC), or propylene carbonate (PC)). The research is conducted using experimental data from the literature such as excess molar enthalpies (H_m^E), volumes (V_m^E), or entropies ($TS_m^E = H_m^E - G_m^E; G_m^E$, molar excess Gibbs energy), and by means of the application of the Flory model and the Kirkwood-Buff integrals. A comparison with the orientational effects present in systems with the corresponding 1-alkanols is also shown. Many of these results were taken from our previous studies on solutions with 1-alkanols [24,26,27]. For the sake of completeness, we have also conducted the needed calculations for 1-propanol, or 1-butanol + acetophenone, or + cyclic diether mixtures, since they have not been previously investigated using the Flory model. Finally, it should be mentioned that different association theories, including a physical term, have been applied to the study of some systems formed by 2-propanol, or 2-butanol and a polar organic solvent (see, e.g., [31–34]).

2. Theories

2.1. Flory model

The main features of the theory are the following [29,35,36]. (i) Molecules are divided into segments, which is an arbitrarily chosen isomeric portion of the molecule. The number of segments per molecule of component i is denoted by r_i and the number of intermolecular contact sites per segment by s_i . (ii) The mean intermolecular energy per contact is proportional to $-\eta/v_s$ (where η is a positive constant characterizing the energy of interaction for a pair of neighbouring sites and v_s is the volume of a segment). (iii) The configurational partition function is stated under the assumption than the number of external degrees of freedom of the segments is < 3 . This is needed to take into account the restrictions on the precise location of a given segment by its neighbours in the same chain. (iv) Random mixing is assumed: the probability of having species of kind i neighbours to any given site is equal to the site fraction, θ_i . For very large total number of contact sites, the probability of formation of an interaction between contacts sites belonging to different liquids is $\theta_1\theta_2$. Under these hypotheses, the Flory equation of state is:

$$\frac{\hat{P}\hat{V}}{\hat{T}} = \frac{\hat{V}^{1/3}}{\hat{V}^{1/3} - 1} - \frac{1}{\hat{V}\hat{T}} \quad (1)$$

where $\hat{V} = V_m/V_m^*$, $\hat{P} = P/P^*$ and $\hat{T} = T/T^*$ are the reduced volume, pressure and temperature, respectively (V_m is the molar volume of the mixture). Equation (1) is valid for pure liquids and liquid mixtures. For pure liquids, the reduction parameters, V_{mi}^* , P_i^* and T_i^* can be obtained from experimental data, such as density, α_{pi} (isobaric expansion coefficient) and κ_{Ti} (isothermal compressibility). For mixtures, the corresponding parameters are calculated as follows:

$$V_m^* = x_1 V_{m1}^* + x_2 V_{m2}^* \quad (2)$$

$$T^* = \frac{\varphi_1 P_1^* + \varphi_2 P_2^* - \varphi_1 \theta_2 X_{12}}{\frac{\varphi_1 P_1^*}{T_1^*} + \frac{\varphi_2 P_2^*}{T_2^*}} \quad (3)$$

$$P^* = \varphi_1 P_1^* + \varphi_2 P_2^* - \varphi_1 \theta_2 X_{12} \quad (4)$$

In equations (3) and (4), $\varphi_i = x_i V_{mi}^* / \sum x_i V_{mi}^*$ is the segment fraction and $\theta_2 = \varphi_2 / (\varphi_2 + S_{12}\varphi_1)$. S_{12} is the geometrical parameter of the mixture, which, in the case of spherical molecules, is calculated as $S_{12} = \left(\frac{V_{m1}^*}{V_{m2}^*}\right)^{-1/3}$. The energetic parameter, X_{12} , also present in equations (3) and (4), is defined, by similarity with $P_i^* = \frac{s_i \eta_{ii}}{2v_s^2}$, as.

$$X_{12} = \frac{s_1 \Delta \eta}{2v_s^2} \quad (5)$$

where $\Delta \eta = \eta_{11} + \eta_{22} - 2\eta_{12}$. In equation (5), v_s^* (reduction volume for segment) and η_{ij} are changed from molecular units to molar units per segments. X_{12} is determined from:

$$H_m^E = \frac{x_1 V_{m1}^* \theta_2 X_{12}}{\hat{V}} + x_1 V_{m1}^* P_1^* \left(\frac{1}{\hat{V}_{m1}} - \frac{1}{\hat{V}} \right) + x_2 V_{m2}^* P_2^* \left(\frac{1}{\hat{V}_{m2}} - \frac{1}{\hat{V}} \right) \quad (6)$$

The reduced volume of the mixture, \hat{V} , is obtained from the equation of state. Therefore, the molar excess volume can be also calculated:

$$V_m^E = (x_1 V_{m1}^* + x_2 V_{m2}^*) (\hat{V} - \varphi_1 \hat{V}_{m1} - \varphi_2 \hat{V}_{m2}) \quad (7)$$

2.2. Kirkwood-Buff integrals

In the framework of this theory [37,38], the Kirkwood-Buff integrals are determined from:

$$G_{ij} = \int_o^\infty (g_{ij} - 1) 4\pi r^2 dr \quad (8)$$

where, g_{ij} is the radial distribution function (probability of finding a molecule of species i in a volume element at the distance r of the center of a molecule of type j). Therefore, g_{ij} provides information about the mixture structure at microscopic level. Values of G_{ij} can be interpreted as follows: positive values represent the excess of molecules of the type i in the space around a given molecule of kind j . That is, attractive interactions between molecules of i and j exist. Negative values of G_{ij} reveal that i - i and j - j interactions are predominant over i - j interactions [37,39]. The Kirkwood-Buff integrals can be derived from thermodynamic data such as chemical potential; partial molar volumes and isothermal compressibility factor. The resulting equations are [37,40]:

$$G_{ii} = RT\kappa_T + \frac{x_j \bar{V}_{mj}^2}{x_i V_{mi} D} - \frac{V_m}{x_i} \quad (i, j = 1, 2)$$

$$G_{12} = G_{21} = RT\kappa_T - \frac{\bar{V}_{m1} \bar{V}_{m2}}{V_m D} \quad (10)$$

where R is the gas constant, x_i and \bar{V}_{mi} are the mole fraction and the partial molar volume of component i , respectively ($i = 1, 2$) and κ_T , the isothermal compressibility of the mixture. D is defined as:

$$D = 1 + \frac{x_1 x_2}{RT} \left(\frac{\partial^2 G_m^E}{\partial x_i^2} \right)_{P, T} \quad (11).$$

The G_{ij} integrals allow estimate the linear coefficients of preferential solvation [41]:

$$\delta_{ii}^0 = x_i x_j G_{ii} - G_{ij} \quad (12)$$

$$\delta_{ij}^0 = x_i x_j (G_{ij} - G_{jj})$$

which are useful quantities to determine the local mole fractions of the i species around the central j molecule [41].

3. Model calculations and results

Values of the properties of pure 2-alkanols and of acetophenone, needed for calculations, are listed in Table 1. For the remainder organic solvents considered, the values used have been taken from previous applications: ketones and organic carbonates [27,42], linear monoethers [24], cyclic ethers [43]. For 1-alkanols, the corresponding values are the same as in reference [25].

3.1. Flory

Table 2 lists values of the interaction parameter X_{12} determined from H_m^E results at equimolar composition and 298.15 K [44] and the source of data used in this application. In addition, the relative standard deviations for H_m^E defined as:

Table 1Physical constants and Flory parameters^a of pure compounds at $T = 298.15\text{ K}$.

compound	$V_{\text{mi}}/\text{cm}^3\text{ mol}^{-1}$	$\alpha_{pi}/10^{-3}\text{ K}^{-1}$	$\kappa_{Ti}/10^{-12}\text{ Pa}^{-1}$	$V_{\text{mi}}^*/\text{cm}^3\text{ mol}^{-1}$	$P_i^*/\text{J cm}^{-3}$
2-propanol	76.96 [112]	1.09 [112]	1147 [112,113]	60.80	454
2-butanol	92.34 [115]	1.03 [114]	995 [114,115]	73.65	485.2
acetophenone	117.44 [117]	0.81 [116]	682 [116,117]	97.27	515.8

^a V_{mi} , molar volumen; α_{pi} , isobaric expansion coefficient; κ_{Ti} , isothermal compressibility, V_{mi}^*, P_i^* , reduction parameter for volume and pressure.

$$\sigma_r(H_m^E) = \left[\frac{1}{N} \sum \left(\frac{H_{m,\text{exp}}^E - H_{m,\text{calc}}^E}{H_{m,\text{exp}}^E} \right)^2 \right]^{1/2} \quad (13)$$

are also given in Table 2 (see Figs. 1–4). Figure S1 (supplementary material) shows the concentration dependence of X_{12} for a few systems. Such dependence has been determined according to the method explained in detail elsewhere [24]. Results provided by the model on V_m^E are collected in Table S1.

3.2. Kirkwood-Buff integrals

Along this type of calculations, isothermal compressibilities of the mixtures were determined from $\kappa_T = \Phi_1 \kappa_{T1} + \Phi_2 \kappa_{T2}$ (where Φ_i is the volume fraction of the component i of the system), i.e., ideal behaviour is assumed. This is a typical approach, which has not influence on the final calculations of the Kirkwood-Buff integrals [45]. Values of D were obtained using Redlich-Kister type expressions for G_m^E determined from vapour-liquid equilibrium (VLE) data at 298.15 K. Results on $\delta_{ij}^0 = x_i x_j (G_{ij} - G_{jj})$ are collected in Table 3 (Fig. 5,6), together with the source of experimental data on VLE and V_m^E used.

4. Discussion

Below, excess molar properties are given at equimolar composition and 298.15 K. On the other hand, X stands for the characteristic functional group of the considered organic solvent, in this study alkanones, ethers or organic carbonates.

Values of H_m^E of 2-alkanol + organic solvent mixtures listed in Table 2 are positive, indicating that interactions between like molecules are dominant. The corresponding V_m^E values are usually positive and therefore the main contribution to this excess function comes from interactional effects. Negative V_m^E values are encountered for a few systems. For example, $V_m^E/\text{cm}^3\text{ mol}^{-1} = -0.247$ (2-propanol + acetophenone) [46]; -0.027 (2-propanol + dipropyl ether) [47] or -0.073 (2-butanol + dipropyl ether) [31]. In such cases, the main contribution to V_m^E arises from structural effects.

4.1. Enthalpies of the hydroxyl-solvent interactions

If structural effects are neglected [48,49], H_m^E can be determined by adding three contributions: two positive, $\Delta H_{\text{OH} - \text{OH}}$, $\Delta H_{X - X}$, due, respectively, to the breaking of alkanol-alkanol and solvent-solvent interactions upon mixing, and a third negative contribution, $\Delta H_{\text{OH} - X}$, related to the new interactions between unlike molecules created along the mixing process. Thus [50–53]:

$$H_m^E = \Delta H_{\text{OH} - \text{OH}} + \Delta H_{X - X} + \Delta H_{\text{OH} - X} \quad (14)$$

The enthalpy of the H-bonds between 2-alkanols and the considered organic solvents, termed as $\Delta H_{\text{OH} - X}^{\text{int}}$ may be evaluated by extending the equation (14) to $x_1 \rightarrow 0$ [53–55]. Then, $\Delta H_{\text{OH} - \text{OH}}$ and $\Delta H_{X - X}$ can be

replaced by $H_{\text{mi}}^{E,\infty}$ (partial excess molar enthalpy at infinite dilution of the first component) of 2-alkanol or organic solvent + heptane mixtures, and H_m^E by the corresponding $H_{\text{mi}}^{E,\infty}$ result of 2-alkanol + organic solvent systems. That is,

$$\begin{aligned} \Delta H_{\text{OH} - X}^{\text{int}} &= H_{\text{mi}}^{E,\infty}(2\text{-alkanol} + \text{organic solvent}) \\ &- H_{\text{mi}}^{E,\infty}(2\text{-alkanol} + \text{heptane}) - H_{\text{mi}}^{E,\infty}(\text{organic solvent} + \text{heptane}) \end{aligned} \quad (15)$$

For 2-alkanol + *n*-alkane mixtures, it was assumed that $H_{\text{mi}}^{E,\infty}$ is independent of the alcohol, a typical approach within association theories [17,56–59]. In this work, we have used $H_{\text{mi}}^{E,\infty} = 23.2\text{ kJ mol}^{-1}$. This is the same value that for mixtures with 1-alkanols [60–62]. The following features support such choice. (i) The direct experimental calorimetric result for the 2-propanol + heptane system at 303.15 K is 23.7 kJ mol^{-1} [63]; for the 2-propanol + cyclohexane mixture at 313.15 K, this value is $H_{\text{mi}}^{E,\infty} = 21.3\text{ kJ mol}^{-1}$ [64]. From H_m^E measurements at 298.15 K over the whole composition range, the $H_{\text{mi}}^{E,\infty}$ values are: 24.7 kJ mol^{-1} for the systems 2-propanol + heptane, or 2-butanol + hexane [65]. (ii) Applications of the ERAS model to mixtures containing 2-alkanols have been conducted assuming that the enthalpy of hydrogen bonding between 2-alkanols molecules is -25.1 kJ mol^{-1} , the same value that for systems with 1-alkanols [17,58,59]. Values of $\Delta H_{\text{OH} - X}^{\text{int}}$ are listed in Table 4. We note that, for mixtures involving a solvent characterized by a functional group X, $\Delta H_{\text{OH} - X}^{\text{int}}$ is, in practice, independent of the alcohol, and of the size of the solvent. $\Delta H_{\text{OH} - X}^{\text{int}}$ results allow conclude that interactions between unlike molecules become stronger in the sequence: linear monoether < linear organic carbonate < *n*-alkanone. On the other hand, alkanol-ether interactions are stronger in the case of cyclic ethers (Table 4).

Values $\Delta H_{\text{OH} - \text{CO}}^{\text{int}}$ have been determined using different theories. The application of an association model including physical interactions described by the NRTL equation yields $\Delta H_{\text{OH} - \text{CO}}^{\text{int}} = -21\text{ kJ mol}^{-1}$ for the 2-propanol + propanone system [32]. In terms of the UNIQUAC-associated solution model [34,66], $\Delta H_{\text{OH} - \text{CO}}^{\text{int}} = -14\text{ kJ mol}^{-1}$ for the 2-butanol + propanone mixture [33], and $\Delta H_{\text{OH} - \text{O}}^{\text{int}} = -16.3\text{ kJ mol}^{-1}$ for the 2-propanol + 1,4-dioxane system [67]. Accordingly to the ERAS model, $\Delta H_{\text{OH} - \text{O}}^{\text{int}} = -18.5\text{ kJ mol}^{-1}$ for the 2-butanol + dipropyl ether mixture [31]. Values obtained using equilibrium constants at different temperatures determined form diamagnetic susceptibility data are [68]: $\Delta H_{\text{OH} - \text{CO}}^{\text{int}}/\text{kJ mol}^{-1} = -17.9$ (2-propanol + propanone); -18.7 (2-propanol + 2-butanol) and $\Delta H_{\text{OH} - \text{O}}^{\text{int}}/\text{kJ mol}^{-1} = -18.7$ (2-propanol + THF). Finally, the value of $\Delta H_{\text{OH} - \text{CO}}^{\text{int}}$ for the 2-butanol + propanone mixture at 303.15 K determined by a thermochemical cycle, which takes into account the dipolar stabilization energy of the 2-butanol-acetone complex, is -17.7 kJ mol^{-1} [69].

4.2. 2-alkanol + *n*-alkanone, or + linear organic carbonate, or + linear ether systems

4.2.1. The effect of increasing the solvent size in mixtures with a given 2-alkanol

At this condition, H_m^E decreases in systems containing a *n*-alkanone, or a carbonate, while H_m^E increases in solutions with linear ethers (Table 2). For example, $H_m^E(2\text{-propanol})/\text{J mol}^{-1} = 1617$ (propanone) [32]; 1504 (2-pentanone) [70]; 962 (dipropyl ether) [47]; 1065 (dibutyl ether) [71]. We note that H_m^E values of 2-alkanol (fixed) + *n*-alkane mixtures increase with the alkane size, and that H_m^E values of the systems *n*-alkanone, or linear organic carbonate, or linear ether + *n*-alkane (fixed) decrease when the size of the polar component increases along each homologous series. Some experimental values are now provided: $H_m^E(2\text{-butanol})/\text{J mol}^{-1} = 885$ (hexane) [65], 1355 (hexadecane) [72] and $H_m^E(\text{heptane})/\text{J mol}^{-1} = 1676$ (propanone) [73]; 1338 (2-butanol)

Table 2

Excess molar enthalpies, H_m^E , at equimolar composition and 298.15 K, for alkanol (1) + organic solvent (2) mixtures. Values of the Flory interaction parameter, X_{12} , and of the relative standard deviations for H_m^E , $\sigma_r(H_m^E)$ (equation (13)) are also included.

System ^a / $X_{12}/\text{J cm}^{-3}$	N^b	$H_m^E/\text{J mol}^{-1}$	$\sigma_r(H_m^E)$	Ref	System ^a / $X_{12}/\text{J cm}^{-3}$	N^b	$H_m^E/\text{J mol}^{-1}$	$\sigma_r(H_m^E)$	Ref
		2-alkanol + ketone					1-alkanol + ketone		
2PrOH + 1CO1 103.86	19	1617	0.082	32	1PrOH + 1CO1 90.12	19	1365	0.038	[118]
2PrOH + 1CO2 88.67	12	1482	0.027	79	1PrOH + 1CO2 75.21	19	1237	0.034	[79]
2PrOH + 1CO3 84.95	10	1504	0.037	70	1PrOH + 1CO3 69.22	19	1209	0.085	[70]
2PrOH + 2CO2 83.00	10	1465	0.053	70	1PrOH + 2CO2 70.74	19	1232	0.101	[119]
2BuOH + 1CO1 106.67	17	1865	0.108	33	1BuOH + 1CO1 89.49	19	1537	0.015	[118]
2BuOH + 1CO2 86.34	13	1630	0.071	80	1BuOH + 1CO2 75.55	19	1421	0.033	[120]
2PrOH + ACP 86.93	12	1568	0.100	97	1PrOH + ACP 75.85	12	1364	0.109	[97]
2BuOH + ACP 108.91	14	2260	0.111	97	1BuOH + ACP 68.80	13	1434	0.099	[121]
		2-alkanol + ether					1-alkanol + ether		
2PrOH + DPE 50.84	14	962	0.274	47	1PrOH + DPE 39.85	13	740	0.377	[47]
2PrOH + DBE 53.07	9	1065	0.393	71	1PrOH + DBE 44.71	21	886	0.414	[122]
2BuOH + DPE 49.58	15	1069	0.219	31	1BuOH + DPE 34.96	12	742	0.346	[105]
2BuOH + DBE 52.68	9	1215	0.235	81	1BuOH + DBE 37.57	27	865	0.363	[122]
2PrOH + THF 68.75	13	1114	0.154	51	1PrOH + THF 58.40	18	933	0.084	[51]
TABLE 2 (continued)									
2PrOH + THP 65.24	18	1119	0.170	51	1PrOH + THP 54.23	17	922	0.185	[51]
2PrOH + 14DX 124.89	19	2066	0.055	51	1PrOH + 14DX 108.10	17	1769	0.037	[52]
2PrOH + 13DX					1PrOH + 13DX 121.56	17	1858	0.039	[123]
2BuOH + THF 62.79	11	1147	0.099	58	1BuOH + THF 51.04	11	927	0.092	[88]
2BuOH + THP					1BuOH + THP 46.79	11	923	0.157	[124]
2BuOH + 14DX 115.16	11	2172	0.057	89	1BuOH + 14DX 105.21	17	1975	0.030	[52]
2BuOH + 13DX 133.95	11	2335	0.035	89	1BuOH + 13DX 115.34	17	2011	0.038	[123]
		2-alkanol + organic carbonate					1-alkanol + organic carbonate		
2PrOH + DMC 133.49	17	2195	0.069	98	1PrOH + DMC 120.34	19	1955	0.073	[98]
2PrOH + DEC					1PrOH + DEC 99.09	19	1794	0.166	[125]
2BuOH + DMC 147.30	17	2743	0.096	99	1BuOH + DMC 126.63	19	2356	0.082	[99]
2BuOH + DEC 109.72	17	2291	0.093	100	1BuOH + DEC 93.19	19	1944	0.134	[125]
2PrOH + PC 144.21	18	2375	0.149	126	1PrOH + PC 130.69	19	2138	0.126	[126]
2BuOH + PC 128.30	17	2405	0.195	126	1BuOH + PC 116.66	19	2200	0.153	[126]

^a symbols are: 2PrOH, 2-propanol; 2BuOH, 2-butanol; 1PrOH, 1-propanol; 1BuOH, 1-butanol; 1CO1, propanone; 1CO2, 2-butanone; 1CO3, 2-pentanone; 2CO2, 3-pentanone; ACP, acetophenone; DPE, dipropyl ether; DBE, dibutyl ether; THF, oxolane; THP, oxane; 14DX, 1,4-dioxane; 13DX, 1,3-dioxolane; DMC, dimethyl carbonate; DEC, diethyl carbonate; PC, propylene carbonate; PC; ^bnumber of data points.

[74]; 1135 (2-pentanone) [74]; 204 (DPE) [75]; 119 (DBE) [76]; 1988 (DMC) [77]; 1328 (DEC) [78]. These results show that H_m^E values of mixtures formed by a given 2-alkanol and a linear ether or *n*-alkane change similarly and that the variation of the H_m^E values of 2-alkanol (fixed) + *n*-alkanone, or + carbonate systems is the same to that of H_m^E of the solutions *n*-alkanone, or + carbonate + *n*-alkane (fixed). That is, alkanol-alkanol interactions are determinant in systems with ethers, while solvent-solvent interactions are determinant in mixtures with *n*-alkanone or carbonate and a given 2-alkanol. In this case, the decrease of

the ΔH_{X-X} term, consequence of the weakening of the dipolar interactions between solvent molecules when their size is increased (see, e.g. [42]), predominates over the increase of the ΔH_{OH-OH} and ΔH_{OH-X} contributions. The former is due to longer solvents are better breakers of the alkanol-alkanol interactions since they have larger aliphatic surfaces. The ΔH_{OH-X} contribution becomes less negative due to the X group is more sterically hindered in longer solvents and a lower number of interactions between unlike molecules are created upon mixing.

On the other hand, H_m^E results of systems involving a given 2-alkanol

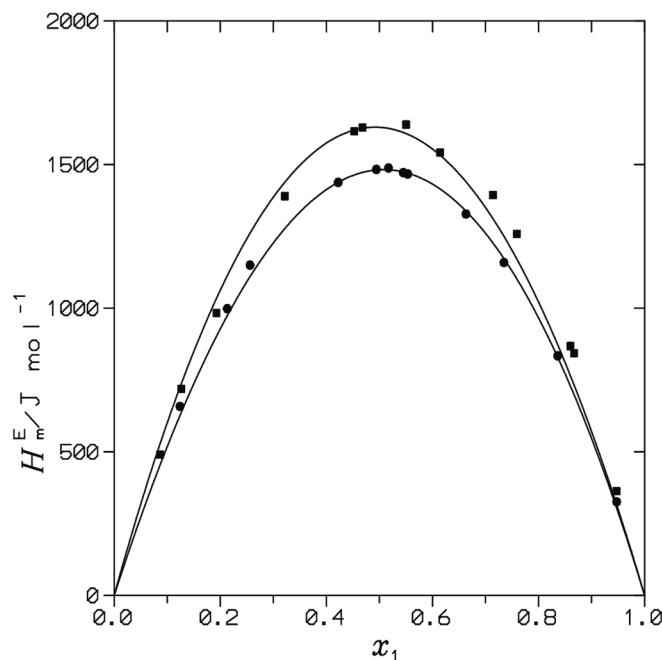


Fig. 1. H_m^E for 2-alkanol (1) + 2-butanone (2) systems at 298.15 K. Points, experimental results: (●), 2-propanol [79]; (■), 2-butanol [80]. Solid lines, Flory calculations with interaction parameters listed in Table 2.

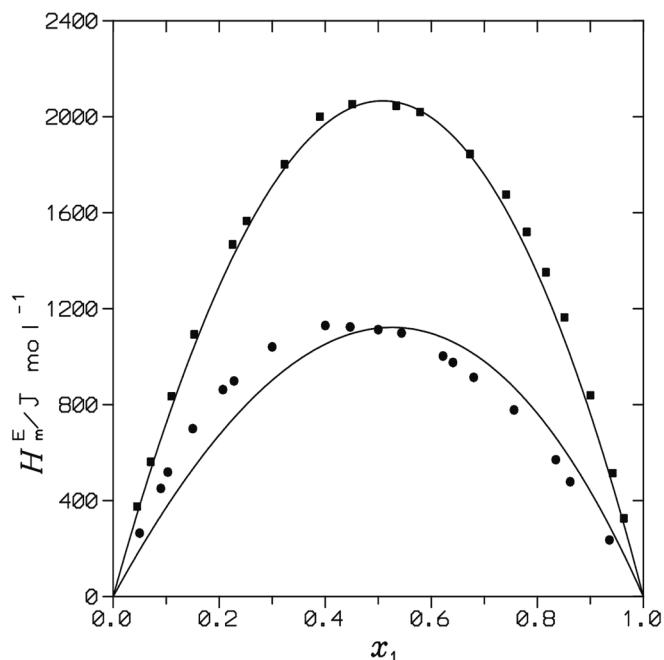


Fig. 3. H_m^E for 2-propanol (1) + cyclic ether (2) systems at 298.15 K. Points, experimental results [51]: (●), oxolane; (■), 1,4-dioxane. Solid lines, Flory calculations with interaction parameters listed in Table 2.

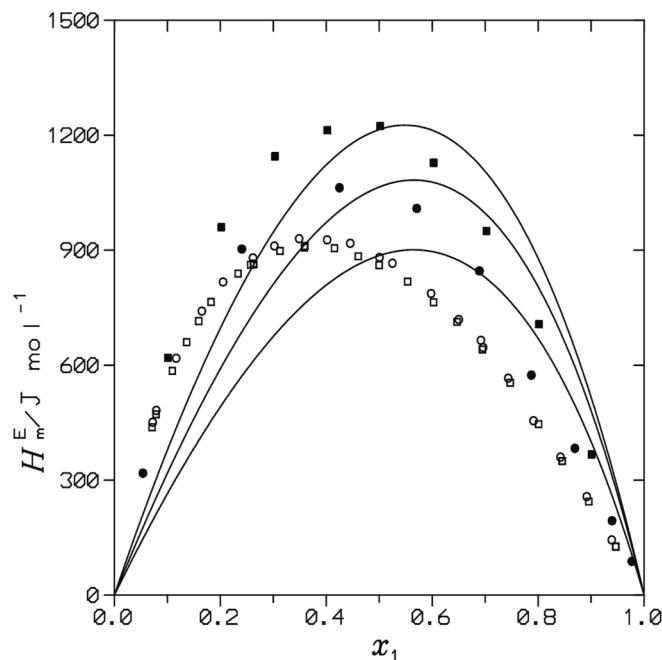


Fig. 2. H_m^E for alkanol (1) + dibutylether (2) systems at 298.15 K. Points, experimental results: (●), 2-propanol [71]; (■), 2-butanol [81]; (○), 1-propanol, 1-butanol [122]. Solid lines, Flory calculations with interaction parameters listed in Table 2.

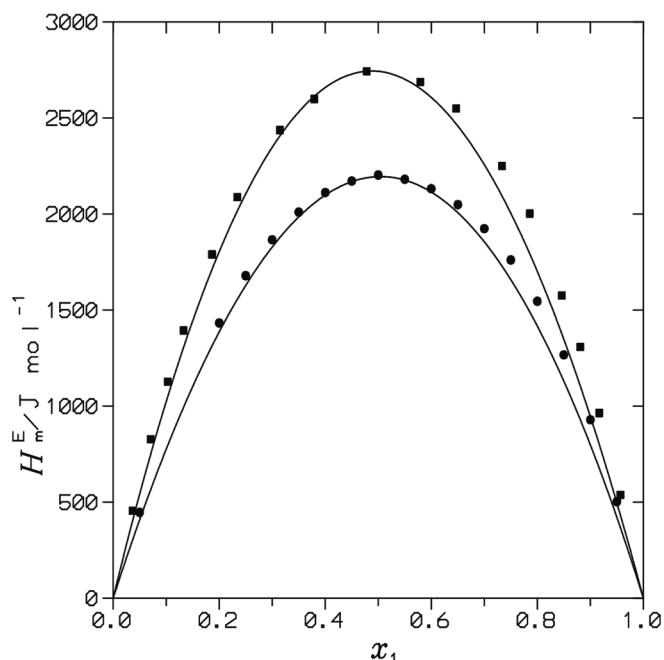


Fig. 4. H_m^E for 2-alkanol (1) + dimethyl carbonate (2) systems at 298.15 K. Points, experimental results: (●), 2-propanol [98]; (■), 2-butanol [99]. Solid lines, Flory calculations with interaction parameters listed in Table 2.

change in the order: organic carbonate > *n*-alkanone > linear ether. This variation is the same that for mixtures formed by one of the mentioned polar compounds and heptane.

The application of the Flory model reveal that values of $\sigma_r(H_m^E) = ((\sum \sigma_r(H_m^E)) / N_S)$; N_S , number of systems) change in the sequence: 0.280 (linear ether) > 0.086 (organic carbonate) > 0.063 (*n*-alkanone). That is, orientational effects become weaker in the

mentioned order, and are much stronger in systems containing ethers, where the alcohol self-association may play a more relevant role. Note that the variation of the X_{12} parameter with the composition is much sharper for the 2-propanol + DPE system than, e.g., in the solution with propanone at 363.15 K (Figure S1). It is interesting to show the values of $T S_m^E (= H_m^E - G_m^E)$ determined using the few experimental G_m^E data available. Thus, $T S_m^E / J \text{ mol}^{-1} = 955$ (2-propanol + 2-butanone) [79], 1174 (2-butanol + 2-butanone) [80], 113 (2-propanol + DPE) [47], 345

Table 3

Linear coefficients of preferential solvation, δ_{ij}^0 , at 2981.5 K and composition x_1 for alkanol (1) + organic solvent (2) mixtures.

System ^a	x_1	$\delta_{11}^0/\text{cm}^3 \text{mol}^{-1}$	$\delta_{12}^0/\text{cm}^3 \text{mol}^{-1}$	Ref.
2-PrOH(1) + DPE(2)	0.2	169.3	- 12.6	[47]
	0.4	173.9	- 44.7	
	0.6	83.7	- 43.2	
	0.8	27.1	- 29.2	
2-BuOH(1) + DPE(2)	0.2	123.2	- 12.1	[31]
	0.4	124.4	- 39.8	
	0.6	60.6	- 39.0	
	0.8	19.2	- 25.0	
2-PrOH(1) + 1CO2(2)	0.2	27.6	- 3.5	[79]
	0.4	36.5	- 15.9	
	0.6	27.9	- 28.4	
	0.8	10.4	- 25.7	
2-BuOH(1) + 1CO2(2)	0.2	18.8	- 5.5	[80]
	0.4	31.8	- 22.8	
	0.6	21.3	- 33.9	
	0.8	4.7	- 20.3	
2-PrOH(1) + THF(2)	0.2	13.2	- 2.3	[127]
	0.4	13.7	- 6.8	
	0.6	7.7	- 8.0	
	0.8	2.4	- 4.9	
1-PrOH(1) + DPE(2)	0.2	159.0	- 9.9	[47,104]
	0.4	164.6	- 39.0	
	0.6	79.5	- 37.9	
	0.8	25.7	- 24.9	
1-BuOH(1) + DPE(2)	0.2	149.9	- 16.1	[105,128]
	0.4	129.5	- 41.6	
	0.6	57.1	- 35.4	
	0.8	18.8	- 24.2	
TABLE 3 (continued)				
1PrOH(1) + 1CO2(2)	0.2	30.7	- 3.5	[79]
	0.4	35.1	- 13.9	
	0.6	25.2	- 23.4	
	0.8	9.9	- 22.8	
1BuOH(1) + 1CO2(2)	0.2	24.5	- 6.6	[111,129]
	0.4	33.9	- 23.8	
	0.6	23.4	- 36.8	
	0.8	6.5	- 28.0	
1PrOH(1) + THF(2)	0.2	16.2	- 3.1	[130]
	0.4	19.4	- 9.3	
	0.6	10.0	- 10.0	
	0.8	2.8	- 5.3	

^a for symbols, see Table 2.

(2-butanol + DPE) [31]. One can conclude that association effects are more important in solutions with ethers. The symmetry of the experimental $H_m^E(x_1)$ curves supports such statement since they are more shifted towards lower mole fractions of the alcohol (x_1) in the case of systems with linear monoethers, while the mentioned curves are more symmetrical for systems involving *n*-alkanones or linear organic carbonates (Figs. 1–4). It is remarkable that the ERAS model has been applied, with rather good results, to 2-alkanol + DPE or + DBE systems [31,71,81]. We have performed ERAS calculations for H_m^E of the 2-propanol + propanone mixture at 298.15 K using the following interaction parameters (determined in this work): $K_{AB} = 60$; $\Delta h_{AB}^* = - 18.5 \text{ kJ mol}^{-1}$; $\Delta v_{AB}^* = - 8.6 \text{ cm}^3 \text{mol}^{-1}$; $X_{AB} = 60 \text{ J cm}^{-3}$. The theoretical $H_m^E(x_1)$ curve is very skewed towards low mole fractions of the alcohol (Figure S2), indicating that the model overestimates the alkanol self-association.

According to the Flory model, positive X_{12} values indicate that interactions between like molecules are prevalent over those between

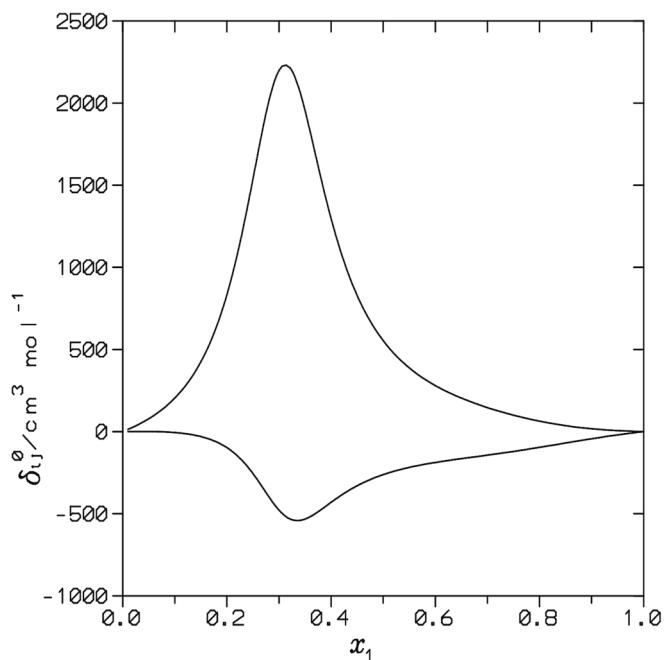


Fig. 5. Linear coefficients of preferential solvation, δ_{ij}^0 , for the 2-propanol (1) + heptane (2) system at 298.15 K. Upper curve, δ_{11}^0 ; lower curve, δ_{12}^0 [92,131].

unlike molecules. Inspection of Table 2 shows that this effect is strengthened in mixtures with linear organic carbonates and that becomes weaker in the order: linear organic carbonate > *n*-alkanone > linear monoether. Along 2-alkanol (fixed) + *n*-alkanone or 2-butanol + linear organic carbonate systems, X_{12} decreases when the solvent size increases. This suggests that the effect linked to the possible decrease of η_{12} is overestimated by that related to the weakening of the dipolar interactions between solvent molecules (η_{22} decrease). In contrast, the former effect is dominant in the systems 2-alkanol (fixed) + linear monoether, and X_{12} increases with the chain length of the oxaalkane.

4.2.2. The effect of replacing 2-propanol by 2-butanol in solutions with a given solvent

At this condition, H_m^E increases (Table 2), which be explained in similar terms that above: i.e., considering that the larger aliphatic surface of 2-butanol breaks more solvent–solvent interactions and that a lower number of interactions between unlike molecules is created along the mixing process when 2-butanol is involved since the OH group is more sterically hindered. Flory results show that $\sigma_r(H_m^E)$ values increase or remains nearly constant when 2-propanol is replaced by 2-butanol in systems with *n*-alkanones or DMC (Table 2). However, in solutions containing linear monoethers, $\sigma_r(H_m^E)$ decreases, which underlines that interactions between 2-propanol molecules are more relevant.

4.3. Acetophenone systems

In view of the available results on H_m^E for 2-alkanol + *n*-alkanone mixtures (Table 2), one can expect that, when comparing H_m^E values of solutions formed by a given 2-alkanol and acetophenone or *n*-alkanone of similar size, the results are higher for the mixtures including the aromatic ketone. In fact, this occurs for 1-alkanol + acetophenone mixtures [82]. Such behavior can be explained considering that the $\Delta H_{\text{CO}-\text{CO}}$ contribution is larger in solutions with acetophenone since its mixtures with *n*-alkane show miscibility gaps at temperatures close to 298.15 K. For example, the upper critical solution temperature (UCST) of the decane system is 277.4 K [82]. As a consequence, $H_m^E(\text{heptane})/\text{J mol}^{-1} = 1493$ (acetophenone) [83], 886 (2-heptanone) [84].

Table 4

Partial molar excess enthalpies at infinite dilution, $H_1^{E,\infty}$, at $T = 298.15$ K at atmospheric pressure for solute(1) + organic solvent(2) mixtures, and hydrogen bond enthalpies, $\Delta H_{\text{OH}-x}^{\text{int}}$, for alkanol (1) + organic solvent (2) systems.

System ^a	$H_1^{E,\infty}$ / kJ mol ⁻¹	$\Delta H_{\text{OH}-x}^{\text{int}}$ / kJ mol ⁻¹	System ^a	$H_1^{E,\infty}$ / kJ mol ⁻¹	$\Delta H_{\text{OH}-x}^{\text{int}}$ / kJ mol ⁻¹
1CO1 + heptane	9.1 [73]				
1CO2 + heptane	7.5 [74]				
1CO3 + heptane	6.4 [74]				
2CO2 + heptane	5.9 [74]				
ACP + heptane	9.2 [83]				
DPE + heptane	0.84 [75]				
DBE + heptane	0.53 [76]				
THF + heptane	3.2 [85]				
THP + heptane	2.2 [85]				
1,4-DX + heptane	7.3 [87]				
1,3-DX + heptane	7.6 [86]				
DMC + heptane	9.5 [77]				
DEC + heptane	7.1 [78]				
2PrOH + 1CO1	7.1 [32]	– 25.2	1PrOH + 1CO1	– 26.0 [26]	
2PrOH + 1CO2	6.0 [79]	– 24.7	1PrOH + 1CO2	– 25.4 [26]	
2PrOH + 1CO3	5.7 [70]	– 23.9	1PrOH + 1CO3	– 22.9 [26]	
2PrOH + 2CO2	7.9 [70]	– 21.2	1PrOH + 2CO2	– 22.1 [26]	
2BuOH + 1CO1	7.5 [33]	– 24.8	1BuOH + 1CO1	– 25.5 [26]	
2BuOH + 1CO2	6.2 [80]	– 24.5	1BuOH + 1CO2	– 25.4 [26]	
2PrOH + ACP	8.0 [97]	– 24.4	1PrOH + ACP	– 25.2 [82]	
2BuOH + ACP	8.3 [97]	– 24.2	1BuOH + ACP	– 24.6 [82]	
2PrOH + DPE	7.3 [47]	– 16.7	1PrOH + DPE	6.5 [47]	– 17.5
2PrOH + DBE	7.2 [71]	– 16.5	1PrOH + DBE		– 16.4 [53]
2BuOH + DPE	8.0 [31]	– 16.0	1BuOH + DPE	4.5 [105]	– 19.5
2BuOH + DBE	7.9 [81]	– 15.8	1BuOH + DBE	7.9 [122]	– 15.9
2PrOH + THF	5.4 [51]	– 21.0	1PrOH + THF	4.5 [51]	– 21.8
TABLE 4 (continued)					
2PrOH + THP	6.0 [51]	– 19.4	1PrOH + THP	4.5 [51]	– 20.9
2PrOH + 1,4DX	8.9 [51]	– 21.6	1PrOH + 1,4DX	7.2 [52]	– 23.3
2BuOH + THF	5.0 [88]	– 21.4	1BuOH + THF	4.4 [88]	– 22.0
2BuOH + 1,4-DX	8.4 [89]	– 22.1	1BuOH + 1,4-DX	7.9 [52]	– 22.6
2BuOH + 1,3DX	10.3 [89]	– 20.5	1BuOH + 1,3DX	9.6 [123]	– 21.2
2PrOH + DMC	9.9 [126]	– 22.8	1PrOH + DMC		– 25.4 [27]
2BuOH + DMC	13.2 [126]	– 19.5	1BuOH + DMC		– 25.3 [27]
2BuOH + DEC	11.2 [126]	– 19.1	1BuOH + DEC		– 19.0 [27]

^a for symbols, see Table 2.

4.4. Cyclization effect

4.4.1. Mixtures with cyclic ethers

Firstly, we note that, in systems including a given 2-alkanol, H_m^E values increase with the number of oxygen atoms of the ether (Table 2). Cyclic ether + heptane systems behave similarly. Thus, $H_m^E(\text{heptane})/\text{J mol}^{-1} = 815$ (THF) [85], 1937 (1,3-dioxolane) [86], 607 (THP) [85], 1784 (1,4-dioxane) [87]. On the other hand, $H_m^E(2\text{-alkanol} + \text{cyclic ether}) > H_m^E(\text{cyclic ether} + \text{heptane})$. For example, $H_m^E(2\text{-butanol})/\text{J mol}^{-1} = 1147$ (THF) [88], 2332 (1,3-dioxolane) [89]. This suggests that 2-alkanols are good breakers of interactions between ether molecules. A similar trend is observed for 2-butanol + DMC mixtures (Table 2).

The application of the Flory model reveals that orientational effects are stronger in systems with THF or THP. Thus, $\bar{\sigma}_r(H_m^E) = 0.118$ (cyclic monoethers), 0.049 (cyclic diethers). One can conclude that in the former mixtures, alkanol-alkanol interactions are more determinant, while in solutions with cyclic diethers interactions are mainly dispersive. Accordingly with this statement, X_{12} remains roughly constant with the composition for the 2-propanol + 1,4-dioxane system (Figure S1). It is to be noted that the $H_m^E(x_1)$ curve of the 2-propanol + THF mixture is more skewed to lower mole fractions of the alcohol than for the corresponding solution with 1,4-dioxane (Fig. 3).

4.4.2. Mixtures with propylene carbonate

These systems are also characterized by large and positive H_m^E values. Note that interactions between propylene carbonate are rather strong in view of the large miscibility gaps of its systems with *n*-alkanes. Thus, at 313.1 K, the propylene carbonate + heptane mixture shows a miscibility gap for mole fractions of the carbonate between (0.001, 0.999) [90]. In contrast, the UCST of the dimethyl carbonate + decane system is 286.6 K [91]. This can explain the stronger orientational effects predicted by the Flory model for 2-alkanol + PC mixtures with regards to those present in systems with DMC or DEC (Table 2).

4.5. Temperature dependence of H_m^E

For the 2-propanol + heptane system, the C_{pm}^E value is large and positive: 15.2 J mol⁻¹ K⁻¹ [92] remarking that the alcohol network is disrupted in large extent when the temperature is increased. This effect is strengthened when heptane is replaced by benzene or toluene. Thus, $(\frac{H_m^E}{\Delta T})_p/\text{J mol}^{-1}\text{K}^{-1} = 17.4$ (benzene), 18 (toluene) [93]. That is, aromatic hydrocarbons are better breakers of the alkanol-alkanol interactions than alkanes. This is supported by the fact that for systems with a given 2-alkanol, say 2-propanol, $H_m^E(\text{benzene}) = 1284$ [93] > $H_m^E(\text{heptane}) = 784$ [94] (values in J mol⁻¹).

4.5.1. Mixtures with ketones or linear organic carbonates

According to experimental data, $(\frac{\Delta H_m^E}{\Delta T})_p(2\text{-propanol})/\text{J mol}^{-1}\text{K}^{-1} = 3.7$ (propanone) [95], 6.1 (2-butaneone) [96], which indicates that association effects are rather weak in these solutions. On the other hand, H_m^E of the 2-propanol + propanone mixture, increases in the temperature range (283.15–323.15) K and decreases at higher temperatures [95], i.e., dispersive interactions become dominant. Systems including acetophenone are characterized by larger $(\frac{\Delta H_m^E}{\Delta T})_p$ values (18.3 J mol⁻¹ K⁻¹ for the solution with 2-propanol [97]). This remarks that aromatic molecules are good breakers of the alcohol network, but also that dipolar interactions between acetophenone molecules are largely disrupted when the temperature is increased. This is supported by the fact that H_m^E values of 2-alkanol + acetophenone mixtures are higher than the corresponding results for 2-alkanol, or acetophenone + hexane or + heptane systems. Thus, for the 2-butanol + acetophenone system, $H_m^E/\text{J mol}^{-1} = 2260$ [97], a value which is much higher than those of the mixtures acetophenone + heptane (1493 J mol⁻¹ [83]) or 2-butanol +

hexane (885 J mol^{-1} [65]). A similar trend is observed for systems with linear carbonates, since the $(\frac{\Delta H_m^E}{\Delta T})_p / \text{J mol}^{-1} \text{ K}^{-1}$ values are also large and positive: 12.7 (2-propanol + DMC) [98]; 11.4 (2-butanol + DMC) [99]; 13.5 (2-butanol + DEC) [100].

4.5.2. Mixtures with cyclic ethers

In this case, the $(\frac{\Delta H_m^E}{\Delta T})_p$ results are lower or even negative. For systems with 2-butanol, such values, in $\text{J mol}^{-1} \text{ K}^{-1}$, are: -0.9 (THF) [88]; 4.0 (1,3-dioxolane); -0.2 (1,4-dioxane) [89]. It is clear that dispersive interactions are here more relatively important.

4.5.3. Flory results at $T > 298.15 \text{ K}$

These results are collected, for a few systems, in Table S2. We note that $\sigma_r(H_m^E)$ values are lower than those obtained for the same mixtures at 298.15 K , showing the typical weakening of the orientational effects when T is increased.

4.6. Excess molar volumes and isochoric excess internal energies

As already stated, most of the systems are characterized by positive V_m^E values (Table S1). In addition, inspection of Tables 2 and S1 shows that H_m^E and V_m^E change in line along a given homologous series. Thus, it is possible to conclude that the main contribution to V_m^E comes from interactional effects. Accordingly, $(\frac{\Delta H_m^E}{\Delta T})_p$ values are positive (Table S1). The Flory model provides much larger V_m^E results than the experimental values (Table S1), indicating that the interactional contribution to this excess function is largely overestimated.

The isochoric molar excess internal energy, U_{Vm}^E can be determined from the equation [48]:

$$U_{Vm}^E = H_m^E - \frac{T \alpha_p V_m^E}{\kappa_T} \quad (16)$$

As in previous applications, we have assumed along calculations that the mixtures show ideal behavior with regards to the expansion coefficient and isothermal compressibility. Table S1 lists the values of U_{Vm}^E determined in this work. Since the $|V_m^E|$ values are usually small, the results of U_{Vm}^E and H_m^E are quite similar, and the relative variations of these magnitudes along a homologous series are also similar. For

example, in the case of mixtures with 2-propanol, $H_m^E / \text{J mol}^{-1} = 1114$ (THF); 1119 (THP) [51] and $U_{Vm}^E / \text{J mol}^{-1} = 1027$ (THF); 1072 (THP). It is interesting to note that the large H_m^E value of the 2-butanol + DMC system (2743 J mol^{-1} [99]) is in part due to structural effects since $U_{Vm}^E = 2474 \text{ J mol}^{-1}$.

4.7. Kirkwood-Buff integrals

We note that the curves δ_{11}^0 vs x_1 , the mole fraction of the alcohol, shows a large maximum for the 2-propanol + heptane mixture at 298.15 K (Fig. 5), which can be ascribed to the alcohol self-association. When the alkane is replaced by a polar compound, the maximum value of δ_{11}^0 largely decreases due to the new alkanol-solvent interactions created upon mixing (Table 3, Fig. 6). This shows that the alcohol network is strongly altered by the presence of a polar compound. For systems including 2-propanol, the mentioned maximum value of δ_{11}^0 decreases in the order: linear monoether > propanone (or 2-butane) > THF (Table 3, Fig. 6). That is, effects related to alkanol-alkanol interactions are much more important in systems with linear monoethers. The symmetry of the $\delta_{11}^0(x_1)$ curve of the 2-propanol + DPE mixture agrees with this statement. The low values of $|\delta_{ij}^0|$ for the solutions with THF, or *n*-alkanone indicate that, in the framework of this model, the behavior of these systems is close to random mixing, since they not form aggregates in solutions. Small preferential solvation effects have previously encountered in systems of alcohols with 1,4-dioxane [101], and somewhat stronger in mixtures with THF [102]. In the case of solutions with linear monoethers, our results suggest that their possible arrangement arises mainly from orientational effects rather than from association effects.

4.8. Comparison with systems containing 1-propanol or 1-butanol

Taking into account the limitations involved in the determination of the $\Delta H_{OH-X}^{\text{int}}$ values, results for mixtures containing 1-alkanols or 2-alkanols are very similar. Nevertheless, data suggest that interactions are stronger in mixtures with DMC. Inspection of Table 2 reveals that the variation of the H_m^E values with the size of the solvent (characteristic group X), or of the 1-alkanol is similar to those previously discussed for

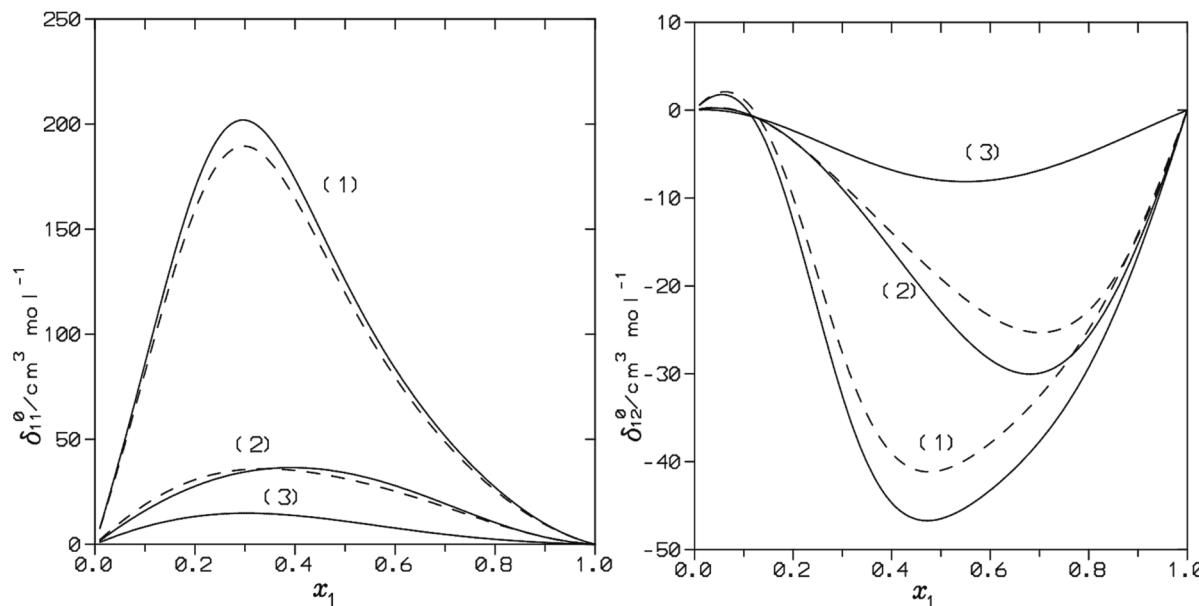


Fig. 6. Linear coefficients of preferential solvation, δ_{ij}^0 , for the alkanol (1) + organic solvent (2) system at 298.15 K . Solid lines, 2-propanol mixtures, dashed lines, 1-propanol solutions: (1), dipropyl ether; (2), 2-butane; (3), oxolane (see Table 3 for source of data).

systems with secondary alcohols, which show larger H_m^E values. This is due to: (i) the ΔH_{OH-X} contribution is more negative for mixtures with 1-alkanols, since the OH group is less sterically hindered [2,58] and more interactions between unlike molecules are created upon mixing. (ii) The ΔH_{OH-OH} contribution is expected to be more positive in systems involving 2-alkanols. Note that for heptane mixtures, $H_m^E/J \text{ mol}^{-1} = 614$ (1-propanol) [103], 784 (2-propanol) [94]. The higher H_m^E values of systems with 2-alkanols lead to the corresponding V_m^E results are also higher. In addition, structural effects are more relevant in systems containing 1-alkanols since, for many systems, values of H_m^E are > 0 , and the corresponding V_m^E results are < 0 , or small in absolute value. For example, $V_m^E(\text{DPE})/\text{cm}^3 \text{ mol}^{-1} = -0.391$ [104] (1-propanol), -0.468 (1-butanol) [105] (the corresponding results for 2-alkanol mixtures are given above); $V_m^E(\text{THP})/\text{cm}^3 \text{ mol}^{-1} = 0.0176$ [106] (1-butanol); 0.282 [107] (2-butanol); $V_m^E(2\text{-butanone})/\text{cm}^3 \text{ mol}^{-1} = -0.0298$ (1-propyl alcohol); 0.2197 (2-propanol) [79]; $V_m^E(\text{DEC})/\text{cm}^3 \text{ mol}^{-1} = 0.292$ (1-butanol); 0.594 (2-butanol) [108]. On the other hand, there is a noticeable difference between the symmetry of the experimental $H_m^E(x_1)$ curves of systems with 1- or 2-alkanols and monoethers, since the former are more skewed to lower mole fraction of the alcohol (x_1) (Fig. 2). This means that association effects are more relevant in the mixtures with 1-propanol or 1-butanol. For the remainder solvents, the symmetry of such curves is quite similar (Figure S2). The values of TS_m^E are consistent with this trend. Thus, $TS_m^E/J \text{ mol}^{-1}$: -74 (1-propanol + DPE) [47]; -14 (1-butanol + DBE) [109,110]; 725 (1-propanol + 2-butanol) [79]; 812 (1-butanol + 2-butanol) [111]. Compare with the results given above for systems with 2-alkanols.

It is remarkable that, according to the results provided by the Flory model, no meaningful difference exists between orientational effects in systems with 1- or 2-alkanols and *n*-alkanone ($\bar{\sigma}_r(H_m^E)(2\text{-alkanol}) = 0.063$; $\bar{\sigma}_r(H_m^E)(1\text{-alkanol}) = 0.051$); or acetophenone ($\bar{\sigma}_r(H_m^E)(2\text{-alkanol}) = 0.105$; $\bar{\sigma}_r(H_m^E)(1\text{-alkanol}) = 0.104$); or cyclic ether ($\bar{\sigma}_r(H_m^E)(2\text{-alkanol}) = 0.095$; $\bar{\sigma}_r(H_m^E)(1\text{-alkanol}) = 0.083$), or linear organic carbonate ($\bar{\sigma}_r(H_m^E)(2\text{-alkanol}) = 0.086$; $\bar{\sigma}_r(H_m^E)(1\text{-alkanol}) = 0.113$). Larger differences exist for systems with propylene carbonate ($\bar{\sigma}_r(H_m^E)(2\text{-alkanol}) = 0.172$; $\bar{\sigma}_r(H_m^E)(1\text{-alkanol}) = 0.139$) and particularly for solutions with linear monoethers ($\bar{\sigma}_r(H_m^E)(2\text{-alkanol}) = 0.280$; $\bar{\sigma}_r(H_m^E)(1\text{-alkanol}) = 0.375$). That is, association effects seem to be more relevant in 1-propanol or 1-butanol + DPE or + DBE systems than in the corresponding mixtures with 2-alkanols. In view of these results, it must be remarked that the dependence of the orientational effects with the functional group is the same along systems with 1- or 2-alkanols. For the solutions considered in Table 3, the formalism of the Kirkwood-Buff integrals does not provide meaningful differences between systems with 1-alkanols or 2-alkanols. This is not the case for 1-propanol or 2-propanol + heptane mixtures at 313.15 K, where the maximum values of $G_{11}(x_1 \approx 0.1)/\text{cm}^3 \text{ mol}^{-1}$ are approximately 11,000 (1-propanol), and 5000 (2-propanol) [23].

Finally, we note that the values of the Flory interaction parameter are larger for mixtures with 2-alkanols, which can be interpreted as consequence of an increase of the 1–1 interactions and a decrease of the 1–2 interactions.

5. Conclusions

Mixtures formed by 2-alkanol and an organic solvent characterized by a polar group (carbonyl, ether, or carbonate) have been studied using experimental data from the literature and by means of the application of the Flory model and the Kirkwood-Buff formalism. It has been shown that dipolar interactions between solvent molecules are determinant in solutions with *n*-alkanones or linear carbonate, and that alkanol-alkanol interactions are determinant in mixtures with linear monoethers. The application of the Flory model reveals that orientational effects in mixtures with a given 2-alkanol become weaker in the order: linear

monoether > linear organic carbonate > *n*-alkanone, and that are stronger in systems with a cyclic monoether than in those with cyclic diethers or in solutions including acetophenone or propylene carbonate than in the corresponding mixtures involving linear solvents. These findings are consistent with results obtained using the Kirkwood-Buff integrals. According to the Flory model, orientational effects are similar in systems with 1- or 2-alkanols, except in the case of solutions with linear monoethers, where such effects are stronger when 1-alkanols are involved. No meaningful differences are encountered between mixtures with 1-alkanols or 2-alkanols when the formalism of the Kirkwood-Buff integrals is applied.

CRediT authorship contribution statement

Juan Antonio González: Conceptualization, Formal analysis, Methodology, Writing – review & editing. **Fernando Hevia:** Formal analysis, Investigation, Validation. **Luis Felipe Sanz:** Conceptualization, Software, Validation, Writing – original draft. **Daniel Lozano-Martín:** Methodology, Investigation, Supervision, Validation. **Isaías García de la Fuente:** Investigation, Supervision, Writing – original draft.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Data availability

The authors do not have permission to share data.

Appendix A. Supplementary material

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.molliq.2023.122319>.

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